


## Sensitivity-based NMPC Strategies for Dynamic Real-time Optimization


L. T. Biegler and Xue Yang  
Department of Chemical Engineering  
Carnegie Mellon University  
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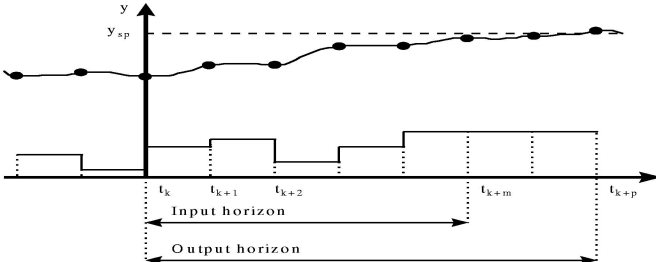
## Outline

- Introduction to NMPC
- Stability Properties of NMPC
- Reducing On-line computation: asNMPC and amsNMPC
- Economic NMPC: ensuring stability and robustness
- Conclusions

2




### Nonlinear Model Predictive Control (NMPC)



$$\min_u J(x(k)) = \sum_{l=0}^N \psi(z_l, u_l) + \Psi(z_N)$$

*s.t.*  $z_{l+1} = f(z_l, u_l)$   
 $z_0 = x(k)$

*Bounds*



### Lyapunov stability of NMPC

- Nominal stability
  - Basic idea
    - Perfect model, no uncertainty:  $x^+ = f(x, u)$
    - Remain bounded and eventually achieve desired state

A function  $V: R^n \rightarrow R_{\geq 0}$  is a Lyapunov function for a system

$$x(k+1) = f(x(k), u(k))$$

if there exist a set  $X$ , three  $\mathcal{K}_\infty$  functions  $\alpha_1, \alpha_2, \alpha_3$  such that

$$\alpha_1(|x|) \leq V(x) \leq \alpha_2(|x|)$$

$$V(f(x, u)) - V(x) \leq -\alpha_3(|x|)$$

$\forall x \in X$

- Can the objective function serve as  $V(x)$ ?

4

### MPC Stability – Infinite Horizon

(Keerthi and Gilbert (1988))

$J_k = \sum_{l=k}^{\infty} \|y(l) - y^{sp}\|_{\sigma^2}^2 + \sum_{l=k}^{\infty} \|u(l) - u(l-I)\|_{\sigma^2}^2$   
 $J_k - J_{k+1} = \|y(k) - y^{sp}\|_{\sigma^2}^2 + \|u(k) - u(k-I)\|_{\sigma^2}^2$   
 $J_1 \geq \sum_{k=1}^{\infty} (J_k - J_{k+1})$   
 $= \sum_{k=1}^{\infty} (\|y(k) - y^{sp}\|_{\sigma^2}^2 + \|u(k) - u(k-I)\|_{\sigma^2}^2)$   
 $\Rightarrow y(k) \rightarrow y^{sp}, u(k) \rightarrow u(k-1)$

**Nominal stability – perfect model**

- Based on discrete Lyapunov arguments with  $J(x)$  as Lyapunov function
- Infinite time horizon, ideal case
- Finite time horizon - need endpoint constraint  $\rightarrow z(k+p)=0$
- Choice of terminal cost gives additional stability properties
- Often  $m$  (input) <  $p$  (output)

15

### NMPC Nominal Stability with Terminal Cost

(Rawlings and Mayne, 2009)

$$\min_u J(x(k)) = \sum_{l=0}^N \psi(z_l, u_l) + \Psi(z_N)$$

s.t.

$$z_{l+1} = f(z_l, u_l)$$

$$z_0 = x(k)$$

**Bounds**

**Assumptions:**

- $f(x, u)$  is Lipschitz continuous (will assume smooth)
- The terminal cost  $\Psi(\bullet)$  satisfies  $\Psi(x) > 0$
- There exists a local control law  $u = \kappa_f(x)$  for all  $x \in X_f$  such that  $\Psi(f(x, \kappa_f(x))) - \Psi(x) \leq -\psi(x, \kappa_f(x))$
- $\psi(x, u)$  satisfies  $\alpha_p(|x|) \leq \psi(x, u) \leq \alpha_q(|x|)$  where  $\alpha_p(\bullet), \alpha_q(\bullet)$  are  $\mathcal{K}$  functions.
- $N$  sufficiently long (Grüne, 2013) or  $\Psi(x)$  sufficiently long (Pannocchia, Rawlings, 2011): no terminal constraints

### Nominal Stability Proof for NMPC

$$J(x(k+1)) - J(x(k))$$

$$\leq \Psi(f(z_N, \kappa_f(z_N))) + \sum_{l=1}^{N-1} \psi(z_l, v_l) + \psi(z_N, \kappa_f(z_N)) - [\Psi(z_N) + \sum_{l=0}^{N-1} \psi(z_l, v_l)]$$

$$= \underbrace{\Psi(f(z_N, \kappa_f(z_N))) - \Psi(z_N) + \psi(z_N, \kappa_f(z_N)) - \psi(z_0, v_0)}_{\leq 0}$$

$$\leq -\psi(z_0, v_0) = -\psi(x(k), u(k))$$

$$J(x(0)) \geq \sum_{k=0}^{\infty} (J(x(k+1)) - J(x(k))) = \sum_{k=1}^{\infty} \psi(x(k), u(k))$$

$$\Rightarrow x(k) \rightarrow 0, u(k) \rightarrow 0$$

- Nominal case** – no noise: perfect model
- Terminal cost**,  $\Psi(z_N)$  – upper bound on control cost for  $z \rightarrow 0$ .
- Robust case** – keep  $(J(x(k)) - J(x(k+1))) > \alpha(x) > 0$  even with noise/mismatch

### Lyapunov stability of NMPC

- Robust stability**
  - Basic idea
    - Uncertainty in model:  $x^+ = f(x, u, w)$ , where  $w$  could be additive disturbance or uncertain parameters;
    - Remain stable in the presence of disturbances.

A function  $V(\cdot)$  is called an ISS-Lyapunov function for a system

$$x(k+1) = f(x(k), u(k)) + q(x(k), w(k))$$

if there exist a set  $X, \mathcal{K}_{\infty}$  functions  $\alpha_1, \alpha_2, \alpha_3$  and a  $\mathcal{K}$  function  $\sigma$  such that

$$\alpha_1(|x|) \leq V(x) \leq \alpha_2(|x|)$$

$$V(f(x, u, w)) - V(x) \leq -\alpha_3(|x|) + \sigma(|w|)$$

$$\forall x \in X, \forall w \in W$$

### Proof of robust stability for NMPC

- Additional Assumptions:
  - $|q(x,w)| \leq |q(x,0)| + L_g |w|$
  - $|q(x,0)| \leq \rho \zeta \alpha_p(|x|)$ , and  $|q(x,0)| \leq q_{max}$ , where  $\rho \in (0,1)$ .

$$\begin{aligned}
 & J(x(k+1)) - J(x(k)) \\
 &= J(f(x(k), u(k))) - J(x(k)) + J(x(k+1)) - J(f(x(k), u(k))) \\
 &\leq -\psi(x(k), u(k)) + L_J |q(x(k), w(k))| \\
 &\leq -\alpha_p(|x(k)|) + L_J \frac{\rho}{\zeta} \alpha_p(|x(k)|) + L_J L_g |w(k)| \\
 &\leq (\rho - 1) \alpha_p(|x(k)|) + \sigma |w(k)|
 \end{aligned}$$

### Nonlinear programming (NLP) formulation for NMPC

$$\begin{aligned}
 J_N(x(k)) &:= \min_{z_l, v_l} \Psi(z_N) + \sum_{l=0}^{N-1} \psi(z_l, v_l) \\
 \text{s.t.} \quad & z_{l+1} = f(z_l, v_l), l = 0, \dots, N-1 \\
 & z_0 = x(k) \\
 & g(z_l) \leq 0, l = 0, \dots, N \\
 & v_l \in U, l = 0, \dots, N-1
 \end{aligned}$$

$z_0$  – initial value  
 $x(k)$  – measurement of state at  $t_k$   
 $\psi, \Psi$  – (quadratic) stage and terminal costs  
 $v_l$  – predicted controlled variable  
 $z_l$  – predicted manipulated variable

How will NLP formulation satisfy assumptions of NMPC stability properties?

### Reformulating the NLP

- Disturbances may lead to infeasibility of the NLP
- Dependent active sets make system unstable under perturbations

- Formulation
  - If  $\epsilon^* = 0$  the stability of the mixed constraint problem is the same as the hard constraint-only problem.

$$\begin{aligned}
 J(x(k)) &:= \min_{z_l, v_l} \Psi(z_N) + \sum_{l=0}^{N-1} \psi(z_l, v_l) + \sum_{l=0}^{N-1} \rho \epsilon_l^T e \\
 \text{s.t.} \quad & z_{l+1} = f(z_l, v_l) \\
 & z_0 = x(k) \\
 & g(z_l) \leq \epsilon_l, \epsilon_l \geq 0 \\
 & v_l \in U, l = 0, \dots, N-1 \\
 & e = [1, 1, 1, \dots, 1]^T
 \end{aligned}$$

Add barrier terms (developed later)

If  $g(z)$  is linear, MFCQ, CRCQ are satisfied at KKT point.  
 → Continuity of  $J(x(k))$  with data perturbations

### Reformulated NMPC Problem

$$\begin{aligned}
 J(x(k)) &:= \min_{z_l, v_l} (\Psi(z_N) - \mu \sum_l \ln(\epsilon_l^{(j)} - g^{(j)}(z_l))) \\
 \text{s.t.} \quad & + \sum_{l=0}^{N-1} (\psi(z_l, v_l) + \sum_j \rho e_l^j e - \mu \sum_j \ln(\epsilon_l^{(j)} - g^{(j)}(z_l))) \\
 & z_{l+1} = f(z_l, v_l), l = 0, \dots, N-1 \\
 & z_0 = x(k) \\
 & \epsilon_l \geq 0, v_l \in U, l = 0, \dots, N-1
 \end{aligned}$$

$v_l := [v_l^T, \epsilon_l^T]^T$   
 $\psi(z_l, v_l) := \psi(z_l, v_l) + \sum_j \rho e_l^j e - \mu \sum_j \ln(\epsilon_l^{(j)} - g^{(j)}(z_l))$

$$\begin{aligned}
 J(x(k)) &:= \min_{z_l, v_l} \Psi(z_N) + \sum_{l=0}^{N-1} \psi(z_l, v_l) \\
 \text{s.t.} \quad & z_{l+1} = f(z_l, v_l), z_0 = x(k), l = 0, \dots, N-1 \\
 & v_l \in U, l = 0, \dots, N-1
 \end{aligned}$$

- Reformulated problem satisfies LICQ for:
  - Bounded multipliers
  - Continuous solutions w.r.t.  $x(k)$
  - Sensitivity

12


**Nonlinear Model Predictive Control – Air Separation Unit**  
(Huang, B., 2011)

**Objective:** maintain product specifications under ramping demands

4 manipulated variables.  
4 output variables.

**Horizon:** 100 minutes in 20 finite elements.  
**Sampling time:** 5 minutes.

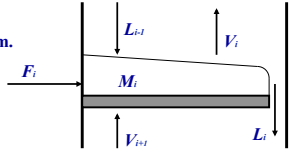
DAEs: 1520  
After Discretization:  
Variables: 117,140  
Constraints: 116,900



**Case Study: Basic Air Separation Unit**

**Mesh Equations for Distillation Column**

**Assumption:**  
Vapor holdups are negligible. Index 2 system.  
Ideal vapor phases.  
Well mixed entering streams.  
Constant pressure drop.  
Equilibrium stage model.



**Mass balance:**  $\frac{dM_i}{dt} = L_{i-1} + V_{i+1} - L_i - V_i + F_i$

**Component balance:**  $\frac{d(M_i x_{i,j})}{dt} = L_{i-1} x_{i-1,j} + V_{i+1} y_{i+1,j} - L_i x_{i,j} - V_i y_{i,j} + F_i x_{i,j}^f$

**Energy balance:**  $\frac{d(M_i h_i^L)}{dt} = L_{i-1} h_{i-1}^L + V_{i+1} h_{i+1}^V - L_i h_i^L - V_i h_i^V + F_i h_i^f$

**Phase equilibrium:**  $y_{i,j} p_i = \gamma_{i,j} x_{i,j} P_{i,j}^{sat}$

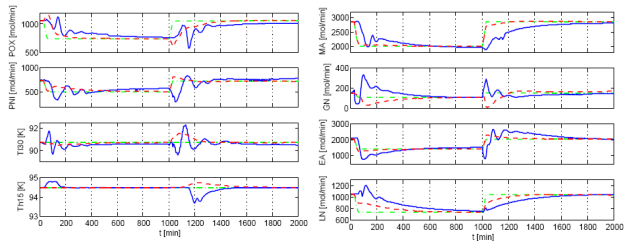
**Hydrodynamics:**  $L_i = k_d M_i$

**Reformulated index 1 system contains 320 ODEs, 1200 AEs.**

**Summation:**  $1 = \sum_{j \in \text{COMP}} y_{i,j}$

**ASU Nonlinear MPC - Case 1**

t = 30-60 min, product rates are ramped down by 30%. t = 1000-1030 min, they are ramped back. NMPC is compared to MPC with linear input-output empirical model.



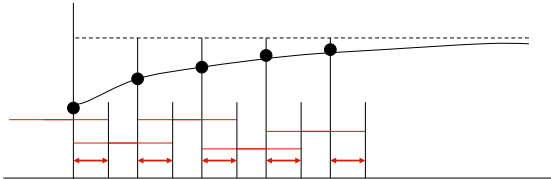
**Output Variables**  
The green dot-dashed lines are the set-points, the blue dashed lines are the linear controller profiles and red solid lines are NMPC profile.

**Manipulated Variables**

All the tuning parameters are favored to the linear controller.  
Horizon Solution Time: 200 CPUs, 6 IPOPT iters.

**What about Fast NMPC?**

- Fast NMPC is not just NMPC with a fast solver (Engell, 2007)
- Computational delay** – between receipt of process measurement and injection of control, determined by cost of dynamic optimization
- Leads to loss of **performance** and **stability** (see Rawlings and Mayne, 2009; Findeisen and Allgöwer, 2004; Santos et al., 2001)



Can computational delay be overcome?  
- Fast Newton-based NMPC  
- Cheap NLP Sensitivity

**NLP Sensitivity**

**Parametric Program**

$$\begin{aligned} \min \quad & f(x, p) \\ \text{s.t.} \quad & c(x, p) = 0 \\ & x \geq 0 \end{aligned} \quad \mathbf{P}(p)$$

**Solution Triplet**

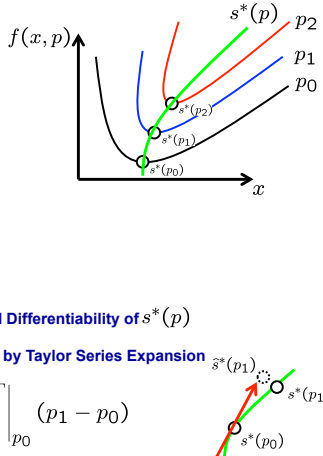
$$s^*(p)^T = [x^{*T} \lambda^{*T} \nu^{*T}]$$

**Optimality Conditions**  $\mathbf{P}(p)$

$$\begin{aligned} \nabla_x f(x, p) + \nabla_x c(x, p) \lambda - \nu &= 0 \\ c(x, p) &= 0 \\ XVe &= 0 \end{aligned}$$

**NLP Sensitivity** → Rely upon Existence and Differentiability of  $s^*(p)$

→ Main Idea: Obtain  $\frac{\partial s}{\partial p} \Big|_{p_0}$  and find  $\tilde{s}^*(p_1)$  by Taylor Series Expansion

$$\tilde{s}^*(p_1) \approx s^*(p_0) + \frac{\partial s^T}{\partial p} \Big|_{p_0} (p_1 - p_0)$$


**KKT Properties and Constraint Qualifications for Sensitivity**

- LICQ, SOSC, SC →  $(ds^*/dp)$  - derivatives can be calculated (Fiacco, 1983)
- MFCQ, GSSOSC, CRCQ →  $(D_{\Delta p} x^*)$  - directional derivatives calculated with additional LP and QP steps (Ralph and Dempe, 1995)
- MFCQ, GSSOSC – continuity of objective functions and primal variables with respect to  $p$ . (Kojima, 1985)

18

**NLP Sensitivity with IPOPT**  
(Pirnay, Lopez Negrete, B., 2011)

**Obtaining**  $\frac{\partial s}{\partial p} \Big|_{p_0}$

**Optimality Conditions of**  $\mathbf{P}(p)$

$$\left. \begin{aligned} \nabla_x \mathcal{L} = \nabla_x f(x, p) + \nabla_x c(x, p) \lambda - \nu &= 0 \\ c(x, p) &= 0 \\ XVe &= 0 \end{aligned} \right\} \mathbf{Q}(s, p) = 0$$

**Apply Implicit Function Theorem to**  $\mathbf{Q}(s, p) = 0$  around  $(p_0, s^*(p_0))$

$$\frac{\partial \mathbf{Q}(s^*(p_0), p_0)}{\partial s} \frac{\partial s}{\partial p} \Big|_{p_0} + \frac{\partial \mathbf{Q}(s^*(p_0), p_0)}{\partial p} = 0$$

$$\begin{bmatrix} W(s^*(p_0)) & A(x^*(p_0)) & -I \\ A(x^*(p_0))^T & 0 & 0 \\ V^*(p_0) & 0 & X^*(p_0) \end{bmatrix} \begin{bmatrix} \frac{\partial x}{\partial p} \\ \frac{\partial \lambda}{\partial p} \\ \frac{\partial \nu}{\partial p} \end{bmatrix} + \begin{bmatrix} \nabla_{x,p} \mathcal{L}(s^*(p_0)) \\ \nabla_p c(x^*(p_0)) \\ 0 \end{bmatrix} = 0$$

**KKT Matrix IPOPT**

$$\begin{bmatrix} W(x_k, \lambda_k) & A(x_k) & -I \\ A(x_k)^T & 0 & 0 \\ V_k & 0 & X_k \end{bmatrix}$$

- Already Factored at Solution
- Sensitivity Calculation from Single Backsolve
- Approximate Solution Retains Active Set

**Updates for active set changes**

- Fix-relax (in sIPOPT)**
  - Bounds are violated → fix  $x^* + \Delta x = x^B \rightarrow \Delta x = x^B - x^*$
  - Multipliers become negative → fix  $v^* + \Delta v = 0 \rightarrow \Delta v = -v^*$
- Clipping in first interval (CFI)**
  - Find step length  $\alpha$  such that
 
$$v^L \leq v_0 + \alpha \Delta v_0 \leq v^U$$

$$z^L \leq z_1 + \alpha \Delta z_1 \leq z^U$$
  - Easiest to implement in asNMPc
- Specialized Linear and Quadratic Programming** (Jäschke et al., 2014)
  - Determine directional derivatives
  - Track family of solutions through homotopy

**Advanced Step Nonlinear MPC** (Zavala, B., 2009)

Solve NLP in background (between steps, not on-line)  
Update using sensitivity on-line

$$\min J(x(k), u(k)) = F(x_{k+N|k}) + \sum_{l=k+1}^{k+N-1} \psi(x_{l|k}, v_{l|k})$$

$$s.t. \quad x_{k+1|k} = f(x(k), u(k))$$

$$x_{l+1|k} = f(x_{l|k}, v_{l|k}), \quad l = k+1, \dots, k+N-1$$

$$x_{l|k} \in X, \quad v_{l|k} \in U, \quad x_{k+N|k} \in X_f$$

Solve NLP(k) in background (between  $t_k$  and  $t_{k+1}$ )

**Advanced Step Nonlinear MPC** (Zavala, B., 2009)

Solve NLP in background (between steps, not on-line)  
Update using sensitivity on-line

$$\begin{bmatrix} W_k & A_k & -I \\ A_k^T & 0 & 0 \\ Z_k & 0 & X_k \end{bmatrix} \begin{bmatrix} \Delta x \\ \Delta \lambda \\ \Delta z \end{bmatrix} = \begin{bmatrix} 0 \\ \vdots \\ x_{k+1|k} - x(k+1) \\ 0 \end{bmatrix}$$

Solve NLP(k) in background (between  $t_k$  and  $t_{k+1}$ )  
Sensitivity to update problem on-line to get  $u(k+1)$

**Advanced Step Nonlinear MPC** (Zavala, B., 2009)

Solve NLP in background (between steps, not on-line)  
Update using sensitivity on-line

$$\min J(x(k+1), u(k+1)) = F(x_{k+N+1|k+1}) + \sum_{l=k+2}^{k+N} \psi(x_{l|k+1}, v_{l|k+1})$$

$$s.t. \quad x_{k+2|k+1} = f(x(k+1), u(k+1))$$

$$x_{l+1|k+1} = f(x_{l|k+1}, v_{l|k+1}), \quad l = k+2, \dots, k+N$$

$$x_{l|k+1} \in X, \quad v_{l|k+1} \in U, \quad x_{k+N+1|k+1} \in X_f$$

Solve NLP(k) in background (between  $t_k$  and  $t_{k+1}$ )  
Sensitivity to update problem on-line to get  $u(k+1)$   
Solve NLP(k+1) in background (between  $t_{k+1}$  and  $t_{k+2}$ )

**Nominal Stability: ideal NMPC and asNMPC**

$$\min_u J_k = \sum_{l=0}^N \psi(z_l, u_l) + F(z_N)$$

$$s.t. \quad z_{l+1} = f(z_l, u_l)$$

$$z_0 = x(k)$$

**Bounds**

$$J_{k-1} - J_k \geq \psi(x(k-1), u(k-1)) + \overbrace{F(z_{Nk-1}) - \psi(z_{Nk}, u_{Nk}) - F(z_{Nk})}^{\geq 0}$$

$$\geq \psi(x(k-1), u(k-1))$$

$$J_0 \geq \sum_{k=1}^{\infty} (J_{k-1} - J_k) = \sum_{k=1}^{\infty} \psi(x(k-1), u(k-1))$$

$$\Rightarrow x(k) \rightarrow 0, u(k) \rightarrow 0$$

- Assumptions:  $f(\cdot)$  is Lipschitz continuous,  $\psi(\cdot)$ ,  $\alpha(\cdot)$  is a  $\chi_{\infty}$  function in  $\|x\|$
- Nominal case – no noise: perfect model
- asNMPC yields identical solutions (no sensitivity perturbation)
  - Identical NMPC stability property

### Robust Stability Margins

**Plant**

$$x_{k+1} = \bar{f}(x_k, u_k) = f(x_k, u_k) + q(x_k, u_k, w_k)$$

$$\|q(x_k, u_k, w_k)\| \leq L_J \|x_k\| + \sigma(\|w_k\|)$$

**Model**

$$z_{j+1} = f(z_j, u_j), z_0 = x_k$$

$$\bar{J}(x_{k-1}) - \bar{J}(x_k) = (\bar{J}(x_{k-1}) - J(z_{k|k-1})) + (J(z_{k|k-1}) - J(x_k)) + (J(x_k) - \bar{J}(x_k))$$

$$\geq \psi(x_{k-1}, u_{k-1}) - \varepsilon(x_k) - \varepsilon_{as}(x_k)$$

$$\geq \psi(x_{k-1}, u_{k-1}) - \varepsilon(x_k) - \varepsilon_{as}(x_k)$$

$$\geq \psi(x_{k-1}, u_{k-1}) - (L_J + L_J K_{as}) / \alpha_g (\|w_{k-1}\|)$$

**Assume above noise and model mismatch model**

- Advanced step NMPC is ISS and tolerates some model mismatch (see Jiang and Wang, 2001; Magni and Scattolini, 2005; Zavala, B., 2009)

17

### Nonlinear Model Predictive Control – Air Separation Unit (Huang, B., 2011)

**Objective:** minimize operating cost subject to demand specifications

4 manipulated variables.  
4 output variables.

**Horizon:** 100 minutes in 20 finite elements.  
**Sampling time:** 5 minutes.

DAEs: 1520  
Variables: 117,140  
Constraints: 116,900  
Background: 200 CPUs, 6 IPOPT iters.  
Online: 1 CPUs

### ASU Nonlinear MPC - Case 1

t = 30-60 min, product rates are ramped down by 30%. t = 1000-1030 min, they are ramped back. asNMPC is compared to MPC with linear input-output empirical model.

**Output Variables**  
The green dot-dashed lines are the set-points, the blue dashed lines are the linear controller profiles and red solid lines are NMPC profile.

**Manipulated Variables**

All the tuning parameters are favored to the linear controller.

### NMPC of Air Separation Unit – Case 2 (Huang, B., 2009)

At t = 30-60 min, product rates are ramped down by 40%.  
At t = 1000-1030 min, they are ramped back. 5% disturbance is added to M<sub>1</sub>.

N = 20, K = 3  
320 ODEs, 1200 AEs.  
Variables: 117,140  
Constraints: 116,900

400 NLPs solved  
Background: 200 CPUs, 6 iters.  
Online: 1 CPUs

Computational Feedback Delay  
Reduced from 200 → 1 second.

Blue dashed lines are ideal NMPC profile  
Red lines are AS-NMPC profile.  
In contrast, linearized controller is unstable

### Advanced Multi-step NMPC (amsNMPC)

- What if NLP solution exceeds one sampling time?
  - Use longer sampling time? Degrades performance
  - Define  $N_s = \text{solution time/sampling time}$ .
  - Do model linearization  $N_s$  steps behind.

**Background:** predict state at  $t(k + N_s)$  and solve NLP using prediction as initial value.  
**On-line:** update  $u(k)$  based on NLP sensitivity at each  $t(k)$ .

**Serial approach:** solve NLP every  $N_s$  sampling times, using one processor.  
**Parallel approach:** solve NLP on  $N_s$  processors at  $t(k)$ .

As  $N_s \rightarrow \infty$ , amsNMPC becomes neighboring extremal controller

X. Yang, L. T. Biegler, Advanced-multi-step nonlinear model predictive control, Journal of Process Control, 23, 2013, pp. 1116-1128

### Parallel amsNMPC, $N_s = 3$

The diagram illustrates the parallel execution of amsNMPC with  $N_s = 3$ . Three processors, NLP1, NLP2, and NLP3, are shown. NLP1 starts at time  $t_k$  and solves for the control  $u(k)$  over a horizon of 3 steps, ending at  $t_{k+3+N}$ . NLP2 starts at  $t_{k+1}$  and solves for  $u(k+1)$  over a horizon of 3 steps, ending at  $t_{k+4+N}$ . NLP3 starts at  $t_{k+2}$  and solves for  $u(k+2)$  over a horizon of 3 steps, ending at  $t_{k+5+N}$ . The state  $x(k)$  is shown as a dashed blue line, and the control  $u(k)$  is shown as a solid red line.

### amsNMPC Case study C3 splitter distillation column

B., Yang, Fischer (2015)

- 158 trays
- 111650 variables
- 111580 constraints
- Horizon length=35
- Sampling time: 1 min

**Assumptions:**  
 Pressure in the column is controlled ;  
 Pressure drop is constant from tray to tray.

The schematic shows a distillation column with 158 trays. Feed enters at tray 43. A Heat Reboiler at the bottom provides vapor to the column. A Heat Condenser at the top provides reflux. Distillate (Propylene) exits from the top. Controlled variables are indicated by blue arrows, and manipulated variables by red arrows.

### Nominal case – no noise

The figure shows four plots comparing ideal NMPC and parallel approach. The top-left plot shows the state  $x(1)$  vs time step, and the top-right plot shows the control  $u(1)$  vs time step. The bottom-left plot shows the states of iNMPC vs parallel approach, and the bottom-right plot shows the control profile of iNMPC vs parallel approach. The plots show that the parallel approach behaves identically to ideal NMPC and amsNMPC.

**States of iNMPC Vs parallel approach**

**Control profile of iNMPC Vs parallel approach**

- Parallel approach behaves identically to ideal NMPC and amsNMPC.
- NLP takes 50 CPUs, Sensitivity update takes less than 0.5 CPUs
- Increasing  $N_s$  does not change performance.



### Noisy case for amsNMPC

- 1% noise in  $x[1]$  and 0.05% noise in  $x[Ntray]$

Set point change, mixed level of noise, parallel approach

States with mixed level of noise

control profile with mixed level of noise

- Parallel amsNMPC can handle a small level of noise with set point change, and for small level of noise  $N_s$  makes no difference.
- As noise increases, more deviation of the states with  $N_s = 3$  than with smaller  $N_s$ .
- Robust performance deteriorates with increasing  $N_s$

### 5% noise in $x[1]$ and 0.1% noise in $x[Ntray]$

- Performance loss with increasing  $N_s$  does not occur because model response to noise is not highly nonlinear.

▶ 34

### Economic NMPC

▶ NLP formulation

$$\min_{z_i, v_i} \Psi(z_N) + \sum_{l=0}^{N-1} \psi(z_l, v_l)$$

s.t.  $z_{l+1} = f(z_l, v_l), l = 0, \dots, N-1$   
 $z_0 = x(k)$   
 $z_l \in X, v_l \in U, l = 0, \dots, N-1, z_N \in X_N$

where  $\Psi(z_N), \psi(z_l, v_l)$  are economic terms  
 Steady state set point is not known -> no terminal region  
 (see Grüne, 2013; Grüne and Stieler, 2014)

▶ Challenge: normally,  $J$  does not satisfy  $\alpha_1(|x|) \leq J(x) \leq \alpha_2(|x|)$

▶ 35

### Challenges with D-RTO

**Replace regulation objective with economic objective in NMPC?**

Bartusiak, Young et al. (2007)  
 Dadhe and Engell (2008), Engell (2007, 2009)  
 Wuerth, Marquardt, Rawlings (2009)  
 Angeli and Rawlings (2010)  
 Angeli, Amrit and Rawlings (2011)  
 Diehl, Amrit and Rawlings (2011)  
 Wolf, Würth, Marquardt (2012)

Robust Stability of Lyapunov function  $\rightarrow$  must be  $\mathcal{K}_{\infty}$  function (e.g., strong convexity of stage cost)

$$\text{Max} \sum_i \{\text{Profit}_i\} + \text{Profit}_N$$

Open Questions

- should D-RTO optimum go to a steady state?
- how do we enforce optimal steady state?

**Remedy: Regularize economic stage cost?**

### Economic NMPC Stability-1

- Economic stage costs generally do not satisfy assumptions for Lyapunov stability e.g.,  $\alpha_p(|x|) \leq \Psi(x, u) \leq \alpha_q(|x|)$
- Obtain steady state solution
 
$$\min \psi(z, v), \text{ s.t. } z = f(z, v), z \in \mathbb{X}, v \in \mathbb{U}$$
- Define transformed states and controls
 
$$\bar{z}_l = z_l - z^*, \quad \bar{v}_l = v_l - v^*$$
- Define rotated stage cost (Diehl, Amrit, Rawlings, 2011)
 
$$L(\bar{z}_l, \bar{v}_l) = \bar{\psi}(\bar{z}_l, \bar{v}_l) + \lambda^{*T} (\bar{z}_l - \bar{f}(\bar{z}_l, \bar{v}_l))$$
- If rotated stage cost is strongly convex at all feasible steady state points, then Lyapunov assumptions are satisfied:
 
$$L(\bar{z}, \bar{v}) \geq 1/2 \int_0^1 [\bar{z}^T \bar{v}^T] \nabla^2 L(\tau \bar{z}, \tau \bar{v}) \begin{bmatrix} \bar{z} \\ \bar{v} \end{bmatrix} d\tau$$

$$\geq \underline{\lambda} (|\bar{z}|^2 + |\bar{v}|^2) \geq \beta_\infty (|\bar{z}|)$$

### Economic NMPC Stability-2

- If rotated stage cost is not strongly convex, add regularization terms to original stage cost
 
$$\psi(z_l, v_l) \Rightarrow \psi(z_l, v_l) + 1/2 \|(z_l - z^*, v_l - v^*)\|_Q^2$$

$$\Psi(z_N) \Rightarrow \Psi(z_N) + 1/2 \|(z_N - z^*)\|_{Q_N}^2$$
- Property 1:** There exists  $Q$  sufficiently large to satisfy Lyapunov assumptions for rotated stage cost
- $Q$  threshold determined from steady state solution
- Property 2:** The NMPC controller with rotated stage costs yields the same control trajectory as with original stage costs. (Diehl, Amrit, Rawlings, 2011)
- Stability and Robustness properties extended to cyclic steady states with  $k$  steps (Huang, Harinath, B; 2012).

### Apply Gershgorin's theorem (Jäschke, Yang, B., 2014)

Recall at steady state optimum  $L(\bar{z}, \bar{v}) \geq 1/2 \int_0^1 [\bar{z}^T \bar{v}^T] \nabla^2 L(\tau \bar{z}, \tau \bar{v}) \begin{bmatrix} \bar{z} \\ \bar{v} \end{bmatrix} d\tau$   
 $\geq \underline{\lambda} (|\bar{z}|^2 + |\bar{v}|^2) \geq \beta_\infty (|\bar{z}|)$

- For a matrix  $A = (a_{i,j}) = \nabla^2 [\psi(z, v) + \lambda^{*T} (z - f(z, v))]$ 

$$a_{i,i} - \sum_{i \neq j} |a_{i,j}| \leq \mu_i \leq a_{i,i} + \sum_{i \neq j} |a_{i,j}|$$
- where  $\mu_i$  is the  $i^{\text{th}}$  eigenvalue of  $A$ .
- To ensure that all the eigenvalues of  $A+Q$  are positive, we require
 
$$0 < q_i + a_{i,i} - \sum_{i \neq j} |a_{i,j}| \leq \mu_i + q_i$$
- therefore
 
$$q_i > \sum_{i \neq j} |a_{i,j}| - a_{i,i}$$
- A+Q should be positive definite for every  $z$  and  $v$ !**

39

### Economic NMPC: Distillation Case study

Two distillation columns in sequence

- 41 trays
- Feed enters at stage 21
- Manipulated variables: LT1, VB1, LT2, VB2
- Additive noise
- Without regularization, the Hessian matrix of Lagrange function of the steady state problem is not positive definite with  $\lambda_{\min} = -1.414$

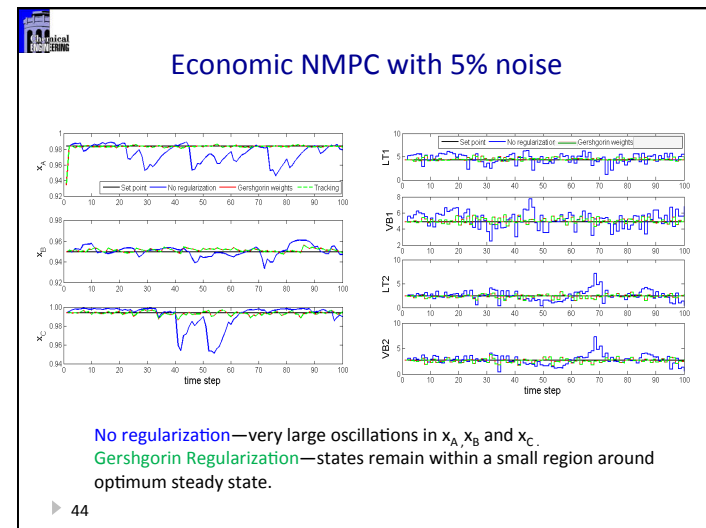
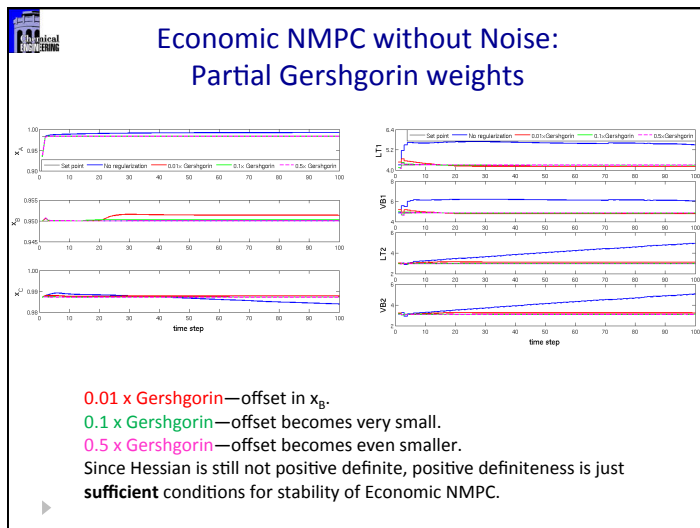
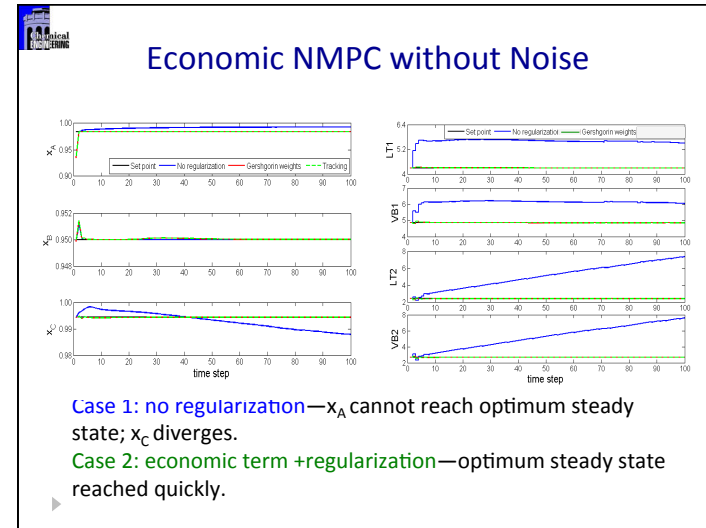
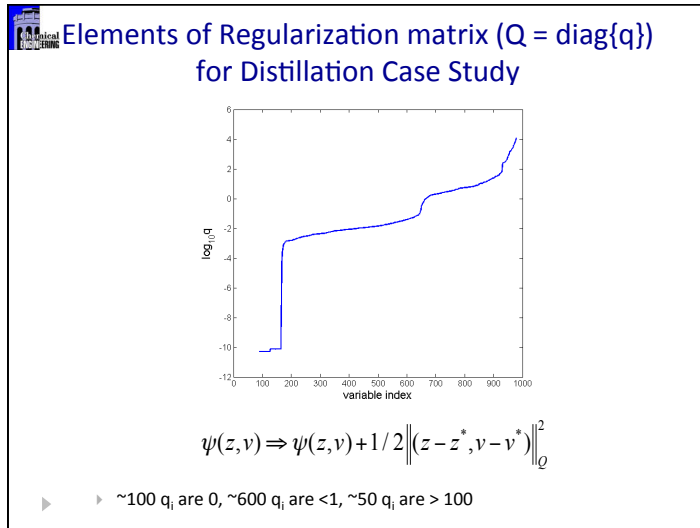
$$\min_u J(u) = p_F F + p_V (VB1 + VB2) - (p_A D1 + p_B D2 + p_C B2)$$

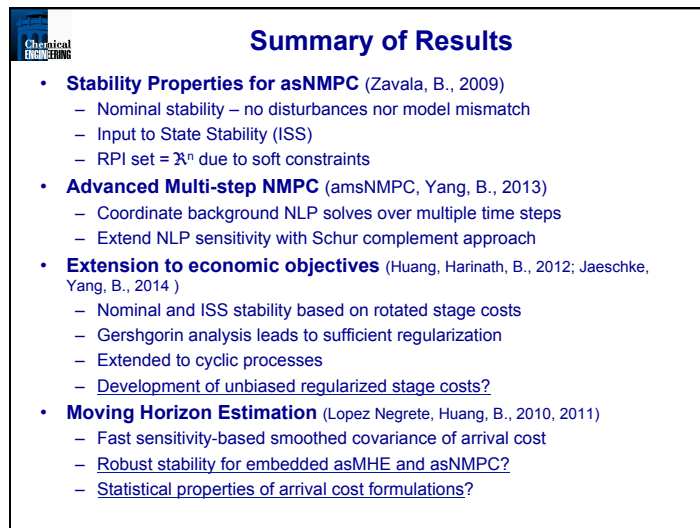
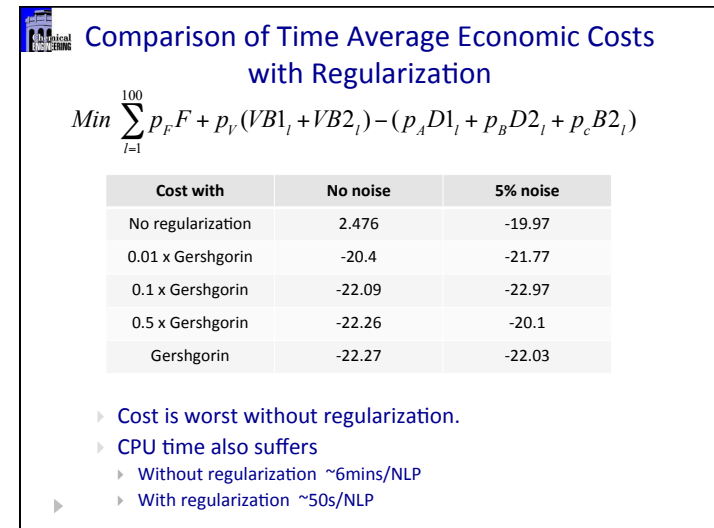
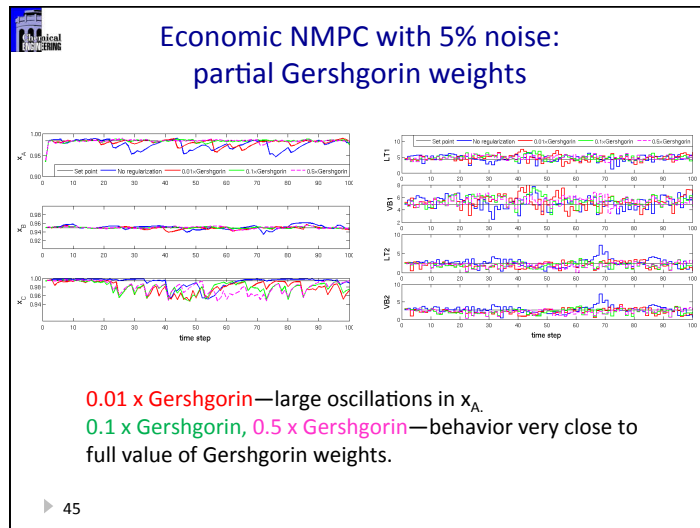
s.t. Massbalance, Equilibrium

$$x_A \geq x_{A,\min}, \quad x_B \geq x_{B,\min}, \quad x_C \geq x_{C,\min}$$

$$0 \leq LT1, LT2 \leq LT_{\max}, \quad 0 \leq VB1, VB2 \leq VB_{\max}$$

Rüß. Leer. Self-optimizing control structures for active constraint regions of a sequence of distillation columns. Master's thesis, Norwegian University of Science and Technology, 2012. Url: <http://www.divaportal.org/smash/get/diva2:629241/FULLTEXT01.pdf>.





### Conclusions

**Sensitivity-based Nonlinear Estimation & Control**

- MHE → asMHE
- NMPC → asNMPC
- RTO → D-RTO

**Bigger NLPs are not harder to solve**

- Embrace and exploit size, sparsity and structure
- Exact first and second derivatives are essential
- Newton-based optimization is fast
- Optimal sensitivity is (nearly) free

**NMPC and MHE Computational Strategies**

- Full-Discretization + Fast Sensitivity Calculations
- Large-scale distillation with nonlinear DAE models

**From NMPC Tracking to Economic Optimization**

- Direct optimization in real-time
- Maintain stability and exploit uncertainties
- Still many open questions

### A Nonrobust NMPC Example (Grimm et al., 2004)

$$\min_{x,u} g(x_{10}) + \rho_g s_N + \sum_{i=0}^{10-1} l(x_i, u) + \rho_l s_i$$

$$s.t. \quad x_1(k+1) = f_1(x, u) = \frac{-(x_1^2(k) + x_2^2(k))^{1/2} u(k) + x_1(k)}{1 + (x_1^2(k) + x_2^2(k)) u^2(k) - 2x_1(k)u(k)}$$

$$x_2(k+1) = f_2(x, u) = \frac{x_2(k)}{1 + (x_1^2(k) + x_2^2(k)) u^2(k) - 2x_1(k)u(k)}$$

$$x_{1,i} \leq c + s_i, i = 0, \dots, N-1, |x_N| \leq \varepsilon + s_N$$

$$u \in [-1, 1], \kappa_f(x) = -1$$

$$g(x) = |x| \cos^{-1} \frac{(x_2 - |x|)(-|x|)}{|x| \sqrt{x_1^2 + (x_2 - |x|)^2}}$$

$$l(x, u) = |x| \cos^{-1} \frac{x_1 f_1(x, -1) + (x_2 - |x|)(f_2(x, -1) - |x|)}{\sqrt{x_1^2 + (x_2 - |x|)^2} \sqrt{f_1(x, -1)^2 + (f_2(x, -1) - |x|)^2}}$$

Grimm, G., Messina, M. J., Tuna, S. and Teel, A. [2004]. 'Examples when nonlinear model predictive control is nonrobust', *Automatica* **40**, 523-533.

### Nonrobust NMPC Example

- ▶ The constraint  $x_1 \leq c$  prevents the trajectory from going beyond  $x_1=c$
- ▶ Soft constraint allows the trajectory to go beyond  $x_1=c$  and then converge

### Economic NMPC Case study: CSTR

$$\min \quad -m(2c_B - \frac{1}{2})$$

$$s.t. \quad \frac{dc_A}{dt} = \frac{m}{V}(c_{Af} - c_A) - kc_A$$

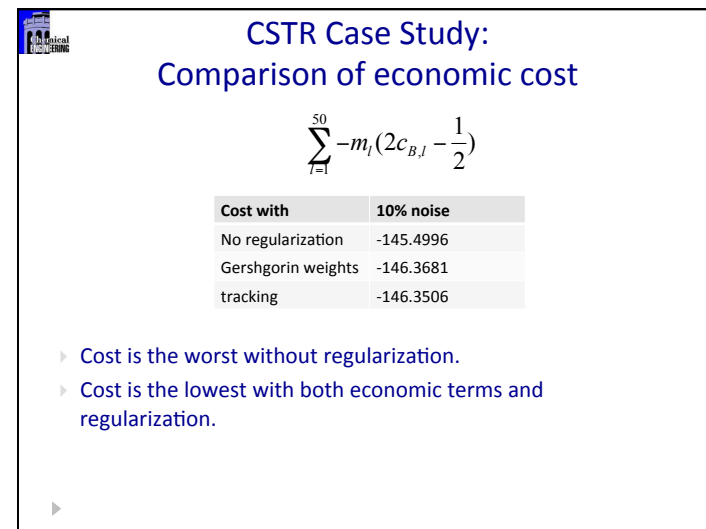
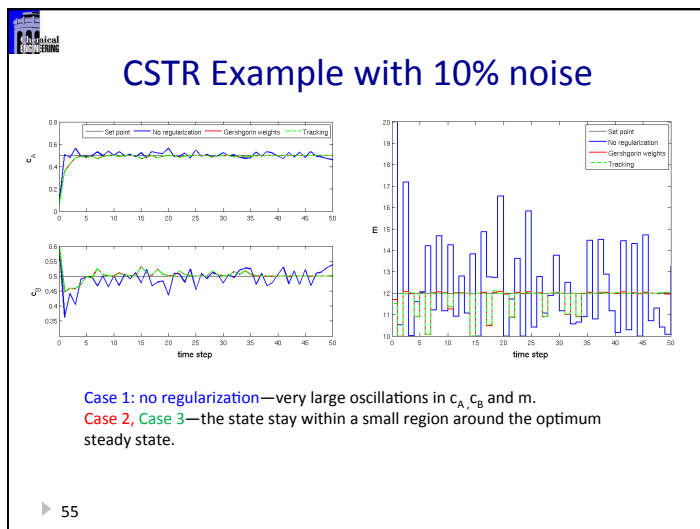
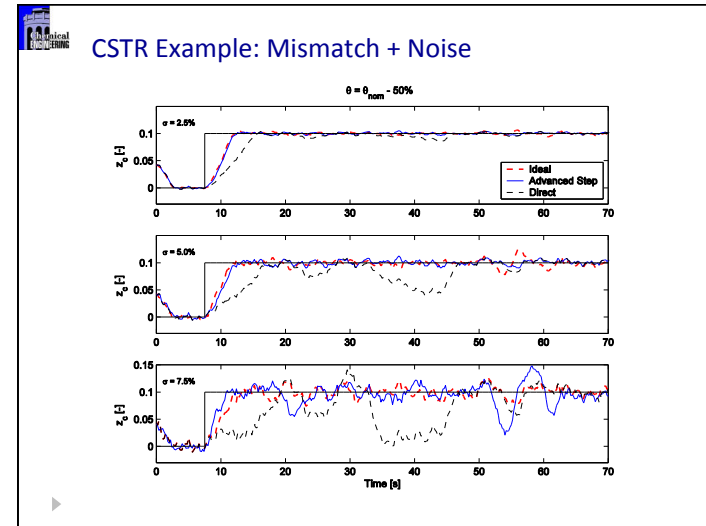
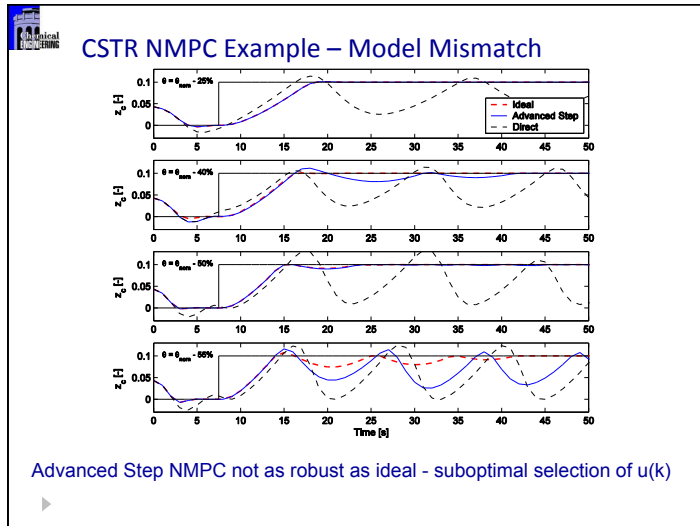
$$\frac{dc_B}{dt} = \frac{m}{V}(-c_B) + kc_A$$

$$10 \leq m \leq 20$$

$$0.45 \leq c_B \leq 1$$

- ▶ First order reaction  $A \rightarrow B$
- ▶  $c_A$  – concentration of A
- ▶  $c_B$  – concentration of B
- ▶  $m$  – manipulated input in L/min
- ▶  $V=10L$
- ▶  $k=1.2L/(mol \cdot min)$
- ▶  $c_{Af}$  – feed concentration
- ▶  $c_{Bf}=1mol/L$

▶ M. Diehl, R. Amrit, J. B. Rawlings, A Lyapunov function for economic optimizing model predictive control, *IEEE Transactions on Automatic Control* 56 (2011) 703-707.



### Advanced-step Economic NMPC

Case 1: ideal NMPC—converges to the setpoint quickly  
 Case 2: asNMPC—control bounds are violated. Strategy not feasible.  
 Case 3: asNMPC + clipping—Avoids control bounds violation. Similar results to ideal NMPC.

► 57

### Recent asNMPC Studies

- Various CSTRs (Zavala, B., 2009)
- NMPC, D-RTO for LDPE reactors (Zavala, B., 2009)
- NMPC, D-RTO for Air Separation Units (Huang, Zavala, B., 2009, 2010; Huang, Patwardhan, B., 2010)
- Large-scale distillation, C3 splitters (Fischer, B., 2011)
- Multi-stage NMPC for power generation cycles (d'Amato, Kumar, Lopez-Negrete, B., 2012)
- Thermo-mechanical pulping (Harinath, B., Dumont, 2010)
- Multi-stage Thermo-mechanical pulping (Harinath, B., Dumont, 2013)
- Advanced multi-step NMPC for distillation control (Yang, Fischer, B., 2013)

58

### CSTR NMPC Example (Hicks and Ray)

$$\min_{v_{1k}} \sum_{l=k}^{k+N-1} Q_c(z_{1k}^l)^2 + Q_c(z_{2k}^l)^2 + R(v_{1k})^2$$

s.t.  $z_{i+1k}^c = \frac{1}{\theta} (1 - (z_{1k}^c + z_{ss}^c)) - k_0 \exp\left(-\frac{E_a}{z_{1k}^c + z_{ss}^c}\right) (z_{1k}^c + z_{ss}^c)$   
 $z_{i+1k}^f = \frac{1}{\theta} (t_f - (z_{1k}^c + z_{ss}^c)) + k_0 \exp\left(-\frac{E_a}{z_{1k}^c + z_{ss}^c}\right) z_{1k}^c - \alpha(v + v_s s) ((z_{1k}^c + z_{ss}^c) - t_c)$   
 $z_{k|k}^c = x^c(k), z_{k|k}^f = x^f(k)$   
 $z_{k+N|k}^c = 0, z_{k+N|k}^f = 0, u^l \leq v_{1k} \leq u^l$

Maintain unstable setpoint  
 Close to bound constraint  
 Final time constraint for stability  
 $z_{k+N|k} = 0, (N \text{ is finite})$

Study effects of:  
 Computational Delay  
 Advanced Step NMPC  
 Measurement Noise  
 Model Mismatch

### CSTR NMPC Example – Nominal Case

- NMPC applied with  $N = 10, \tau = 0.5$  sampling time
- Stable ( $z = 0$ ) and unstable ( $z = 0.1$ ) steady states
- $u_2^*$  close to upper bound
- Computational delay = 0.5, leads to instabilities
- asNMPC has identical performance as Ideal NMPC

**asNMPC: Concepts and Properties**

- Interpretation: Fast linear MPC controller using *linearization of nonlinear model at previous step*.
- NLP solved between samples, “instantaneous” sensitivity update at sampling time
- On-line computation 2-3 orders of magnitude faster;
  - ➔ Computational delay virtually eliminated
- Second order errors compared to ideal NMPC
  - ➔ Nominal and ISS stability (Zavala, B., 2009)
- ISpS stability when coupled with embedded state estimators (Huang, Patwardhan, B., 2009a,b, 2010a-c, 2012)

**Advanced-multi-step NMPC**

- Motivation: what if the solution of NLP takes more than one sampling time?
  - Slow down sampling?

62

**Summary: Advanced-(multi) step NMPC**

- Avoids computational delay
- Allows solving NLP  $\geq$  one sampling time
- Behaves close to ideal NMPC and asNMPC with small level of measurement noise and less nonlinear model
- With increasing noise, process nonlinearity and  $N_s$ , memory effect becomes more significant
- Robustness could be obtained by using soft constraints and adding  $\ell_1$  penalty to the objective. Moreover, robustness is preserved when amsNMPC is applied, under additional assumptions on memory effect

**Dynamic On-line Optimization:**

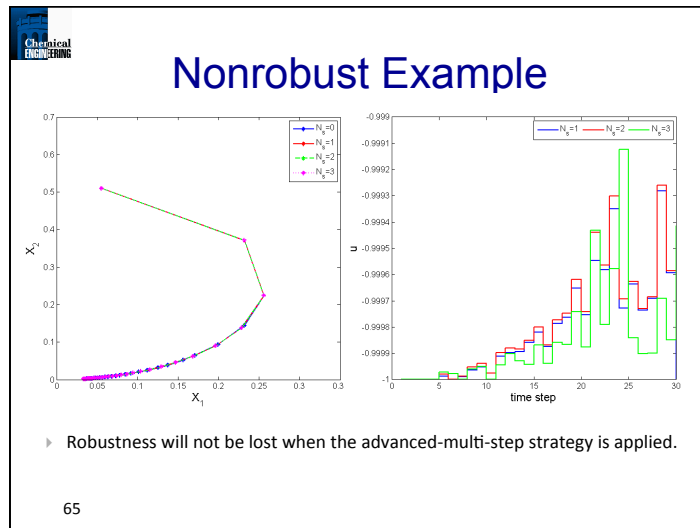
*Integrate On-line Optimization with APC*

- Consistent, first-principle dynamic models
- Consistent, feed-forward optimization
- Increase in computational complexity
- Time-critical calculations

*Essential for:*

- Feed changes
- Nonstandard operations
- Optimal disturbance rejection





**Stability Properties of asNMPC**

$x(k+1) = f(x(k), u(k))$  – plant and model identical

**Nominal Stability Theorem** (Zavala, B., 2008)

Assume that the NLP can be solved within one sampling time, nominal stability assumptions hold for ideal NMPC (Mayne, 2000), and the nonlinear model is perfect without measurement noise. Then ideal NMPC controller performance and asNMPC controller performance are identical. Ideal NMPC stability  $\rightarrow$  asNMPC stability.

$x(k+1) = f(x(k), u(k)) + g(x(k), u(k), w(k))$   
plant and model not identical

**Robust Stability Theorem** (Zavala, B., 2008)

Assume that the NLP can be solved within one sampling time, and that robust stability assumptions hold for ideal NMPC (Magni, Scattolini, 2007). Then there exist bounds on the noise,  $w$ , and model mismatch,  $g$ , for which the cost function  $J_{N+1}(x)$ , obtained from the asNMPC strategy, is an input-to-state (ISS)-Lyapunov function and the resulting closed-loop system is ISS stable.

**NMPC – Can we avoid on-line optimization?**

- **Divide Dynamic Optimization Problem** (Diehl, Bock et al., 2002):
  - preparation, feedback response and transition stages
  - solve complete NLP in background ( ‘between’ sampling times) as part of preparation and transition stages
  - solve perturbed problem on-line
  - > two orders of magnitude reduction in on-line computation
- **Based on NLP sensitivity of  $z_0$  for dynamic systems**
  - Extended to Collocation approach – Zavala et al. (2008, 2009)
  - Similar approach for MH State and Parameter Estimation – Zavala et al. (2008)
- **Stability Properties** (Zavala et al., 2009)
  - Nominal stability – no disturbances nor model mismatch
    - Lyapunov-based analysis for NMPC
  - Robust stability – some degree of mismatch
    - Input to State Stability (ISS) from Magni et al. (2005)
  - Extension to economic objective functions